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Alicyclobacillus acidoterrestris spore inactivation by high pressure combined with mild heat: Modeling the effects of temperature and soluble solids

Rafael Uchida, Filipa V.M. Silva



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1 *Alicyclobacillus acidoterrestris* spore inactivation by high pressure combined with mild heat:

2 Modeling the effects of temperature and soluble solids

3

4 Rafael Uchida, Filipa V.M. Silva*

5 Department of Chemical and Materials Engineering, University of Auckland, Private Bag

6 92019, Auckland 1142, New Zealand.

7 * Corresponding author Filipa Silva. Tel: +64 9 3737999, Fax: +64 9 3737463, Email:

8 filipavinagresilva@gmail.com.

9

10 **Abstract**

11 High pressure processing (HPP) comprises the application of pressures between 100-1000
12 MPa to foods for microbial inactivation and food preservation. HPP has been commercially
13 applied to pasteurize fruit juices with the advantage of retaining its bioactive constituents and
14 original organoleptic properties. *Alicyclobacillus acidoterrestris* has been suggested as a
15 reference in the design of pasteurization for high-acid fruit products, due to spore resistance
16 and spoilage incidents in fruit juices. In this study, *A. acidoterrestris* spore inactivation by
17 600 MPa combined with mild heat (35-65°C) in malt extract broth adjusted to 10, 20 and
18 30°Brix was carried out and the inactivation was modeled.

19 The soluble solids increased the resistance of the spores to 600 MPa-thermal process, while
20 the temperature decreased its resistance. Although the nonlinear Weibull model gave better
21 fittings, the first-order kinetic parameters were also determined. For example for 600 MPa at
22 55°C $D_{10^{\circ}\text{Brix}} = 4.2$ min, $D_{20^{\circ}\text{Brix}} = 7.6$ min, $D_{30^{\circ}\text{Brix}} = 13.7$ min, and z_T -values were 20-21°C.
23 The z -values for the effect of soluble solids on D_T -values were 39–40 °Brix for 45 and 55°C
24 600 MPa HPP. The results obtained with broth were validated with fruit juices and
25 concentrates. The combination of HPP with heat was an effective alternative to conventional

26 thermal processing for the inactivation of *A. acidoterrestris* spores in juices up to 30°Brix,
27 allowing the use of less 30-40°C of temperature for the same microbial inactivation, which
28 potentially results in more nutritious, fresher and tastier juices/concentrates.

29

30 **Keywords:** acidophilic, high pressure thermal processing, *Alicyclobacillus acidoterrestris*,
31 fruit juices, fruit concentrates, Brix.

32

33

34 **1. Introduction**

35 Although the first scientific publication demonstrating the extension of milk shelf life by
36 high pressure processing (HPP) dates back to 1899 (Hite, 1989), its commercial scale was
37 initiated in 1990 in Japan to produce three different jams (Hayashi, 1995). There are several
38 successful high pressure processed products sold globally (Rastogi, 2013): fruit juices, jams,
39 jellies, rice cakes and raw squids in Japan; salsa, guacamole meal kits, oysters in shells,
40 ready-to-eat meat in the US; fruit juices, especially apple and orange juice in France,
41 Portugal, Italy, UK, Mexico and the USA; and apple sauce in Canada. High hydrostatic
42 pressure (HPP) is another term used for the same technology, since water is used to surround
43 and transmit the pressure to the food uniformly and rapidly (Hayashi, 1989). Although HPP is
44 mostly used for the inactivation of microorganisms and enzymes (Sulaiman, Soo, Yoon,
45 Farid, & Silva, 2015), the technology can also be applied for protein gelation, cold
46 denaturation of proteins, freezing and thawing of foods, or meat tenderization (San Martín,
47 Barbosa-Cánovas, & Swanson, 2002). Molecules such as amino acids, vitamins, responsible
48 for flavor, and low molecular weight are hardly affected by the process. As a consequence,
49 the organoleptic and nutritional properties are retained with the process, and HPP treated food
50 presents higher quality (Rendueles, et al., 2011).

51 *Alicyclobacillus acidoterrestris* is an acidophilic, thermophilic, non-pathogenic, Gram-
52 positive, strictly aerobic, spore-forming bacterium which has been related to several spoilage
53 incidents in a variety of products such as apple juice (Cerny, Hennlich, & Poralla, 1984),
54 shelf stable iced tea containing berry juice (Duong & Jensen, 2000) and carbonated fruit
55 drink (Pettipher & Osmundson, 2000). Therefore it has been suggested as reference
56 microorganism to design pasteurization processes in acidic fruit products (Silva, Gibbs,
57 Vieira, & Silva, 1999; Silva & Gibbs, 2001; 2004; 2009; Silva, Gibbs, Nunez, Almonacid, &
58 Simpson, 2014). The microorganism cell is rod-shaped measuring 2.9 – 4.3 μm long and 0.9
59 – 1.0 μm wide and the oval-shaped spores are 1.5 – 1.8 μm long and 0.9 – 1.0 μm wide
60 (Walker & Phillips, 2008), both able to grow between 25 – 60°C (optimum: 42 – 53°C) and
61 low pH (Pontius, Rushing, & Foegeding, 1998; Yamazaki, Teduka, & Shinano, 1996). One of
62 the main challenges related to the specific spoilage by *A. acidoterrestris* is the difficulty to be
63 identified, since it is not linked with acid or gas production. The most evident signs of
64 spoilage are the off-flavor and off-odor, described as “medicinal, phenolic and antiseptic” due
65 to the production of 2-methoxyphenol, the guaiacol (Yamazaki, et al., 1996) and other
66 halophenols. One of the most distinctive characteristic of *Alicyclobacillus spp.* is the presence
67 of ω -alicyclic fatty acids as the principal membrane component. Research demonstrated these
68 closely packed fatty acids contribute to the heat resistance of the microorganism when a
69 protective layer with strong hydrophobic bonds is formed. In extreme acidic and high
70 temperature environment, these bonds stabilize and reduce the membrane permeability
71 (Jensen, 1999; Kannenberg, Blume, & Poralla, 1984). The thermal processing D-value at
72 95°C of endospores of different *A. acidoterrestris* strains in fruit juices vary between 1.5 and
73 8.7 min (Eiroa, Junqueira, & Schimdt, 1999; Evelyn & Silva, 2016a; Silva & Gibbs, 2001).

74

75 Bacterial spores are also extremely resistant to HPP. It has been accepted the impossibility to
76 achieve high levels of *Bacillus*, *Clostridium* and mold spore inactivation by applying pressure
77 alone in the commercial range of 200 to 600 MPa (Black, et al., 2007; Evelyn & Silva, 2015a,
78 2015b, 2016b; 2016c; Evelyn, Kim, & Silva, 2016). Therefore, HPP combined with mild heat
79 is recommended: HPP-thermal or HPTP (high pressure thermal processing). The mechanism
80 of spore inactivation by HPP is not completely known. It has been postulated that spores
81 germinate first under certain temperature/pressure conditions, losing their resistance and
82 readily inactivated by the HPP treatment. Under very high pressure (400 to 800 MPa), there
83 is an induced spore germination accompanied by the release of dipicolinic acid with calcium
84 – Ca-DPA (Rendueles, et al., 2011; Wuytack, Boven, & Michiels, 1998). The release of Ca-
85 DPA leads to cortex lysis, possibly due to the effects on DPA channels in the inner
86 membrane or on the spore's membrane itself (Black et al., 2007). After germination, spores
87 are much more sensitive to agents such as heat, pH and pressure compared to the dormant
88 state (Hongkang & Mittal, 2008).

89
90 In the fruit juice/concentrates industry, soluble solids (expressed in °Brix) is one of the most
91 important parameters, given its influence on the microbial resistance to pressure and heat
92 (Basak, Ramaswamy, & Piette, 2002; Palou, et al., 1998; Silva, et al., 1999). The inactivation
93 of *A. acidoterrestris* spores by HPP and HPTP in fruit juices and concentrates has barely been
94 explored, with only a few studies found in the literature (Lee, Dougherty, & Kang, 2002; Lee,
95 Chung, & Kang, 2006; Silva, Tan, & Farid, 2012; Sokołowska, et al., 2012, 2013). There is
96 no literature report on modeling the effect of soluble solids on the inactivation of *A.*
97 *acidoterrestris* spores using combined HPP and thermal processing (HPP-thermal or HPTP)
98 in fruit juice concentrates. Therefore the objectives of this research were: (1) to model the
99 HPP-thermal inactivation of *A. acidoterrestris* spores in 10, 20 and 30 °Brix broths, (2) to

100 investigate the effect of HPP temperature and soluble solids on the spore inactivation, (3) to
101 validate the model with commercial fruit juice concentrates.

102

103

104 **2. Material and methods**

105 2.1. *Alicyclobacillus acidoterrestris* microbiology

106 2.1.1. *Strain and growth medium*

107 A freeze dried strain of *Alicyclobacillus acidoterrestris* NZRM 4447 (New Zealand
108 Reference Culture Collection, Medical Section) was acquired from the Institute of
109 Environmental Science and Research (ESR) in New Zealand. This is the type strain, same as
110 ATCC 49025^T, NCIMB 13137^T, DSM 3922^T, GD3B^T and CIP 106132^T. The culture was
111 grown for 3 days at 45°C on potato dextrose agar (PDA) (BD Difco, North Ryde, Australia)
112 adjusted to pH 4.0 after sterilization with 0.1 g/mL of tartatic acid.

113

114 2.1.2. *Spore production*

115 Fresh culture was spread onto PDA adjusted to a pH of 5.6 and incubated at 45°C for 21 days
116 or until at least 80% of the cells were sporulated. Sporulation was monitored by microscope
117 examination after staining with 0.005 g/mL safranin and 0.05 g/mL malachite green
118 solutions. When the desired sporulation was obtained, the spores were harvested by adding 1
119 to 2 mL of sterile water onto PDA plates and gently removing the surface growth with a
120 sterile inoculator. The suspensions obtained from 20 plates were centrifuged at 4000 g for 20
121 min at 4°C (Centrifuge Sigma 4K15, UK) and the pellet was resuspended in sterile water and
122 centrifuged again at 4000 g for 10 min at 4°C. This last step was repeated 3 more times to
123 wash the spores. The final pellet was resuspended in sterile sodium phosphate buffer (pH 7.2)
124 and stored at 4°C until use.

125

126 *2.1.3. Spore enumeration*

127 In order to determine the spore concentration (N), a serial dilution technique was used, where
128 0.1 mL of spore suspension was diluted with 0.9 mL of sterile water in test tubes down to a
129 dilution of 10^{-6} . The test tubes were vortex mixed before taking a portion for further dilution
130 to ensure uniform concentration of spores. After the dilution, test tubes were heated at 80°C
131 for 10 min in a water bath to destroy any remaining vegetative cells. For each tube dilution, 2
132 x 0.1 mL was spread plated in two PDA plates (pH 4.0) and incubated at 45°C for 3 days.
133 After incubation, the colonies formed (cfu) were counted when ranging between 30 – 300 cfu
134 and the average counts were calculated for each dilution and spore concentration was
135 expressed in cfu/mL.

136

137 *2.2. Preparation of broth, juices and concentrates for HPP-thermal processing*

138 The malt extract broth (MEB) (BD Difco, North Ryde, Australia) was adjusted to 10, 20 and
139 30°Brix by adding sucrose crystal and using a refractometer (Atago, Abbe Refractometer
140 DR-A1, Japan). The pH was adjusted to 3.8 using a pH meter (Mettler Toledo, S20 –
141 SevenEasy, USA) with a 10% w/v (0.1 g/mL) solution of tartatic acid (Univar, Ajax
142 Finechem, Australia). The MEB solution was then sterilized using the autoclave. A small
143 volume (0.1 mL) of spore suspension was added to the sweetened MEB to reach a
144 concentration of ca. 10^6 CFU/mL. Several 6 cm x 10 cm transparent retort pouches (Cas-Pak,
145 New Zealand) were filled with 2 mL of the inoculated MEB and thermosealed under vacuum
146 (Multivac C200, Germany). The plastic film was composed by polyester coated with silicon
147 oxide, laminated to nylon and laminated to cast polypropylene
148 (PETSIOX(12)/ON(15)/RCPP(70)). These bags were 1.0 mm thick, presented a low oxygen
149 transmission rate ($< 2 \text{ cc/m}^2/24 \text{ h}$) and could withstand temperatures up to 130°C , appropriate

150 for high pressure thermal processing. The same packaging film was used for fruit juice and
151 concentrate samples.

152

153 2.3. Experimental design

154 First, packed MEB samples with different soluble solids (10, 20 and 30°Brix) were submitted
155 to HPP combined with mild temperature (T) of 35, 45, 55, and 65°C with processing times (t)
156 up to 45 min. A 600 MPa HPP pressure was selected, the maximum pressure (P) allowed by
157 the equipment, since HPP by itself is not sufficient for *A. acidoterrestris* spore inactivation
158 (Lee, et al., 2002; Silva, et al., 2012). Two samples were processed for each P-T-t and soluble
159 solids content conditions and the average \pm standard deviation of log survivors was plotted.

160 To validate the spore inactivation results, commercial apple juice and fruit juices concentrates
161 were submitted to 600 MPa HPP combined with 45°C. The soluble solids were adjusted in
162 the fruit juice concentrates by dilution with sterilized water. Apple juice (10.6°Brix,
163 pH=3.38), adjusted lime juice concentrate (20.2°Brix, pH=2.50) and adjusted blackcurrant
164 concentrate (30.3°Brix, pH=3.05) were processed and *A. acidoterrestris* spore inactivation
165 was compared with 10, 20 and 30°Brix MEB, respectively. HPP-thermal processing and
166 spore inoculation/enumeration were carried out as described previously.

167

168 2.4. High Pressure Processing (HPP)

169 The HPP unit Avure 2 L Laboratory Food Processing System (Avure Technologies,
170 Columbus, Ohio, USA) was used. The machine can operate at a maximum temperature and
171 pressure of 90°C and 600 MPa, respectively. The equipment comprises a 2 L cylindrical
172 shaped pressure treatment chamber pumping system, water circulation for heating and is
173 controlled by a software provided by the manufacturer through a desktop computer. During
174 the process, the chamber containing the packed MEB, fruit juice or concentrate samples, was

175 filled with distilled water. The chamber was equipped with two thermocouples which
176 registered the water temperature during the HPP treatment inside the chamber. A pre-heating
177 of the pressurized fluid (distilled water) inside the chamber was required. The treatment time
178 considered for the experiment was the holding pressure time and did not include the
179 pressurization and depressurization phases. The pressure come up time to reach 600 MPa was
180 approximately 1.5 min and adiabatic heating was observed during this period, resulting in
181 approximately 5°C higher than the average/target temperature during the constant pressure
182 phase. During the pressure holding phase (isobaric), a decrease in the chamber temperature
183 was registered. Care was taken to adjust the initial temperature of the water inside the
184 pressure vessel in order to obtain an average temperature during the treatment as close as
185 possible to the desired treatment temperature. The depressurization time was approximately
186 30 sec. After treatment the broth/juice samples were immediately cooled in ice water. The
187 spore counting was carried out as described in section 2.1.3.

188

189 2.5. Modeling the kinetics of *A. acidoterrestris*

190 The survival curves of log of spores numbers versus time were plotted for modeling the data.
191 The microbial survivors for thermal inactivation usually follow the first-order kinetic, with
192 log linear reduction of the microorganism population. However, several studies reported
193 deviations from linearity (e.g., tail, biphasic curves, concave and convex curves) in survival
194 curves of different microorganisms, especially after HPP. Below are the two models used in
195 this study.

196

197 2.5.1. First-order kinetic

198 HPP-thermal inactivation of microorganisms' population is dependent on the treatment time
199 at a constant pressure and temperature, and expressed in number of viable spores. For each

200 pressure-temperature condition, the inactivation can be modeled by the following equation:

$$201 \quad \log\left(\frac{N}{N_0}\right) = -\frac{1}{D_T}t \quad (1)$$

202 where N is the final number of viable spores (cfu/mL) at time t (min), N_0 is the initial
 203 population of spores (cfu/mL) at time zero, and $\log(N/N_0)$ is the number of log reductions in
 204 spores during the processing time t . For first order kinetics the log of the spore ratio (N/N_0) is
 205 linear with time, and the slope of the survival curve is $-1/D_T$. The decimal reduction time D_T ,
 206 is defined as the time in minutes to achieve one log cycle reduction in the spore
 207 concentration. D_T is temperature (T)/soluble solids content (SS) dependent according to the
 208 following equations:

$$209 \quad \log\left(\frac{D_T}{D_{ref}}\right) = \frac{T_{ref}-T}{z_T} \quad (2)$$

$$210 \quad \log\left(\frac{D_{SS}}{D_{ref}}\right) = \frac{SS_{ref}-SS}{z_{SS}} \quad (3)$$

211 where the z_T - and z_{SS} -values are the increase of temperature and soluble solids that reduces
 212 D_T by a factor 10, respectively.

213

214 2.5.2. Weibull model

215 The Weibull equation has been successfully used to model the inactivation of several
 216 microorganisms by different processes (Evelyn & Silva, 2015a, 2015b, 2015c; Evelyn, et al.,
 217 2016; Weibull, 1951). This model considers that spores have different resistances (as opposed
 218 to the first-order kinetic) and a survival curve represents the cumulative form of a distribution
 219 of lethal agents. The Weibull model distribution is represented by the following equation:

$$220 \quad \log\left(\frac{N}{N_0}\right) = -bt^n \quad (4)$$

221 where b and n are the scale and shape parameters respectively (Peleg & Cole, 1998).
 222 Normally for HPTP $n < 1$, and the survival shape is concave upward. When $n = 1$ is linear
 223 (equal the first-order kinetic, Equation 1) and if $n > 1$ a concave downward is registered.

224

225 *2.5.3. Data analysis and model performance*

226 The *A. acidoterrestris* spore logarithmic reduction ($\text{Log } N/N_0$) was calculated and the average
227 was plotted for each HPP-thermal processing time. The linear and several nonlinear models
228 (Weibull, modified Gompertz and Log-Logistic) were attempted using the software
229 *TableCurve 2D* (Systat, USA). The goodness of fit of the models was assessed by the
230 coefficient of determination (R^2) and the mean square error (MSE). Weibull was the best
231 model, and b and n parameters \pm standard error were estimated (Eq. 4). In addition the first-
232 order kinetic parameter D_T and z -values were also estimated to compare with previous results.

233

234

235 **3. Results and discussion**236 **3.1 HPP-thermal inactivation of *A. acidoterrestris* in broth**

237 The *A. acidoterrestris* spores survival lines in broth after HPP at 600 MPa combined with
238 mild temperature (35, 45, 55 and 65°C) for different soluble solids content (10, 20 and
239 30°Brix) are presented in Figures 1 and 2. The higher the temperature/soluble solids content,
240 the higher the spore inactivation. A 2.3 decimal reduction was obtained for 10°Brix after
241 HPP-55°C-10 min, and a value of 2.8 log reductions was obtained for 20°Brix MEB after
242 HPP-65°C-7 min and for 30°Brix after HPP-65°C-10 min. Thermal processing by itself
243 without HPP cannot achieve any inactivation of *A. acidoterrestris* spores at these
244 combinations of °Brix/temperatures. For example Evelyn and Silva (2016a) worked with the
245 same strain in 9.5°Brix orange juice, and obtained less than 0.1 log reductions after 10 min at
246 78°C, the lowest temperature tested. Silva et al (1999) determined 0.15 log reduction of *A.*
247 *acidoterrestris* type strain spores in 32.5°Brix broth after 10 min thermal treatment at 85°C,
248 the lowest temperature tested.

249

250 *3.1.1. Effect of HPP temperature*

251 The HPP temperature has a significant role in the inactivation of *A. acidoterrestris* spores.
252 When the temperature increased, the rate of microbial destruction also increased (Fig. 1). For
253 instance, 5 min treatment at 600 MPa at 55°C resulted in an approximately 1.2 log reduction
254 of *A. acidoterrestris* spores in MEB 10°Brix, while at 35°C more than 45 min was needed to
255 obtain the same degree of inactivation. Previous NZRM 4098 *A. acidoterrestris* spore
256 inactivation suspended in orange juice (9.2°Brix) processed by 600 MPa-45°C-10 min
257 (Silva, et al., 2012) was similar to our experiment with 10°Brix MEB with type strain (around
258 1 log reduction). At 600 MPa-55°C, while after 5 min the log inactivation results in orange
259 juice and broth were similar (~1.2), for 10 min processing time the log reduction in broth
260 almost double the value to 2.2. Studies with a cocktail of NFPA1013 and NFPA1101 strains
261 17.5°Brix apple juice subjected to 621 MPa-45°C resulted in approximately 2.2 and 2.5 log
262 reductions after 5 and 10 min, respectively (Lee et al., 2006). Our inactivation with NZRM
263 4447 in 20°Brix MEB processed for 10 min at 600 MPa-45°C was much lower, with a value
264 of 0.6 log reduction.

265

266 *3.1.2 Effect of soluble solids*

267 Figure 2 shows the effect of soluble solids on the 600 MPa-55°C *A. acidoterrestris* spore
268 inactivation. After 10 minutes the results for 10, 20 and 30°Brix broth were respectively 2.2,
269 1.1 and 0.5 log reductions. Therefore, when applying HPP-thermal process in to fruit
270 concentrates, and similar to thermal resistance alone, the higher the soluble solids content, the
271 lower the spore inactivation, demonstrating a protective effect. Concentrated juice with high
272 soluble solids presents a low water activity. Clearly, water availability has an effect on the
273 reaction of microorganisms to high pressure thermal treatment (Lee, et al., 2006). The

274 baroresistance may be in part explained by the incomplete spore germination under low water
275 availability conditions (Black, et al., 2007). Other authors observed the same baroresistance
276 in apple juice/concentrate (Lee, et al., 2002; Sokołowska, et al., 2013), although no modeling
277 was attempted.

278

279 3.2. Modeling the HPP-thermal inactivation of *A. acidoterrestris* spores in 10, 20 and 30

280 °Brix broths

281 An upward concavity was observed for 10 and 20°Brix broths, while downward concavities
282 were registered for 30°Brix at 45 and 55°C. The possible explanation is that the
283 microorganism populations are composed by several subpopulations, each one presenting
284 distinct inactivation patterns, which causes the nonlinear curves (van Boekel, 2002).
285 Furthermore, previous authors postulated the spore number and age, protoplast dehydration
286 and sporulation temperature might also affect HPP-thermal resistance (Chang & Kang, 2004;
287 Jay, Loessner, & Golden, 2005). The best fitting was obtained with the Weibull model,
288 presenting in general higher R^2 and lower MSE than the first order kinetics (Tables 1 and 2).

289

290 3.2.1. Nonlinear Weibull model

291 The Weibull model fitting for the inactivation curves of *A. acidoterrestris* by combined high
292 pressure and mild heat is represented in Fig. 1. These curves indicates that the Weibull model
293 fits were very satisfactory, confirming the performance indices shown on Table 1. The shape
294 factor (n) less than 1 (Table 1), confirmed the upward concavity of the *A. acidoterrestris*
295 survival curves at 10 and 20°Brix, except 10°Brix - 35°C which was close to linear $n=1$. The
296 $n<1$ means that the remaining cells have less chance of dying, being most resistant ones, or
297 maybe the cells have the ability to adapt to the stress. Therefore, the concave upward might
298 be understood as evidence of quick inactivation of the weak or sensitive cells of the

299 populations and the remaining survivors were the sturdy ones. Similar upward trend was
300 observed with HPP-thermal of orange juice (Silva et al., 2012). On the contrary, a downward
301 concavity ($n > 1$) for 30° Brix broths was obtained at 45 and 55°C. In addition, no change or a
302 slight decrease trend in n was observed with the HPP temperature. Buzrul et al. (2005)
303 reported at certain pressures, shape parameter was dependent on temperature. Van Boekel
304 (2002) reported in only 7 out of 55 studies n seemed to be dependent on temperature. Cunha
305 et al. (1998) suggested the shape parameter n should indicate the kinetic pattern of the model
306 that controls the process studied and thus, be independent from the external factor,
307 temperature.

308 Regarding the scale parameter b from the Weibull equation, also known by the rate
309 parameter, a linear increase of $\log b$ with T of the HPP-thermal process was noted (Fig. 3),
310 analogous to $1/D_T$ -value. Evelyn and Silva (2015a) observed the same log-linear trend for b
311 parameter of *B. cereus* HPP-thermal inactivation in milk and temperature dependency was
312 also registered in HPP-thermal inactivation of spores of *Byssochlamys nivea* and *Neosartorya*
313 *fischeri* moulds in fruit products (Evelyn and Silva, 2015b; Evelyn et al., 2016).

314

315 3.2.2 Linear first order kinetics

316 The D_T -values were estimated for different HPP temperatures and broths soluble solids
317 contents from the reciprocal of the slope of log-survivor versus treatment time (Table 2). As
318 expected the D_T -values decreased with temperature. For 10° Brix, at 35, 45 and 55°C the D_T -
319 values were 38.08, 10.32 and 4.17 min, respectively. Previous 600 MPa HPP-thermal
320 inactivation studies carried out with a different *A. acidoterrestris* spore strain (NZRM 4098)
321 in orange juice (9.2°Brix and pH=3.8) resulted in: $D_{45^\circ\text{C}}$ -value =12.9 min and $D_{55^\circ\text{C}}$ = 7.0 min
322 (Silva, et al., 2012). The z_T -values for 10, 20 and 30°Brix at 600 MPa were similar to the
323 three soluble solids broths ranging from 20 to 21°C. The usual z -value for thermal process

324 alone is approximately half 7-13°C (Silva & Gibbs, 2009), this being an indication of lower
325 susceptibility to temperature change in a HPP-thermal process than a thermal process.

326 The protective effect of soluble solids is evident reaching around threefold increase from 4.2
327 min at 10°Brix-55°C to 13.7 min at 30°Brix-55°C. The z -value can also be calculated for
328 constant temperature and varying soluble solids content (Equation 3). In order to reduce one
329 \log_{10} in the D_T value, it is necessary to reduce approximately by 38-40°Brix (z_{SS} -value) the
330 soluble solids content.

331

332 3.3 Model validation with commercial fruit juices/concentrates

333 Table 3 shows a comparison of HPP-thermal inactivation results in MEB and fruit
334 juices/concentrates for 10, 20 and 30°Brix. The results were good and both models
335 parameters were similar for broth and real fruit products. For example, D_T -value obtained
336 with 10°Brix MEB/apple juice and 20°Brix MEB/lime juice from concentrate were 9-10 min
337 and 20-22 min, respectively. Regarding 30°Brix blackcurrant juice concentrate, the D_T -value
338 in MEB was lower than the corresponding fruit concentrate. However, very close b and n
339 were obtained when using Weibull model.

340

341

342 4. Conclusion

343 Although in conventional thermal processes, a temperature of $\geq 95^\circ\text{C}$ is required for *A.*
344 *acidoterrestis* spore inactivation, much lower temperatures of 45 to 65°C were needed when
345 using HPP-thermal technology. This can represent more retention of original fruit
346 organoleptic properties, nutrients and bioactive components, which address the current
347 consumers demand for fresher, healthier, convenient and tastier foods.

348 *A. acidoterrestris* spores are very resistant to HPP-thermal processes. Similar to thermal
349 processing we have demonstrated the higher the temperature of the 600 MPa HPP-thermal
350 process and the lower the soluble solids content of the medium processed, the higher was the
351 inactivation of *A. acidoterrestris* spores. For example 1.2 log reductions was obtained in
352 10°Brix broth after 5 min-55°C, 10 min-45°C and 45 min-35°C, 2.0-2.3 log reductions was
353 observed in 20°Brix broth, after 2.5 min-65°C, 15 min-55°C and 45 min-45°C, and regarding
354 30°Brix, 1.5 to 1.9 log reductions were observed after either 7.5 min-65°C, 20 min-55°C or
355 45 min-45°C.

356 The *A. acidoterrestris* inactivation under 600 MPa HPP combined with mild heat was well
357 modelled with Weibull model, however first order kinetics was also reasonable. The $D_{55^{\circ}\text{C}}$ -
358 value was 4.17, 7.59 and 13.71 min in 10, 20 and 30°Brix broths, respectively, showing the
359 protective effect of the soluble solid content against HPP-thermal process. The z_T -value of
360 20-21°C was similar for the three different soluble solids investigated and the z_{SS} -value for
361 the soluble solids was 38-40°Brix. The model predictions from experiments with broth were
362 validated with commercial fruit juices/concentrates, which showed close HPP-thermal
363 inactivation results between broths and commercial juices of analogous soluble solids
364 content.

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Table 1. Weibull b and n parameters and model performance for *A. acidoterrestris* spores inactivation by 600 MPa HPP combined with mild heat in malt extract broth adjusted 10, 20 and 30°Brix.*

Soluble solids (°Brix)	HPP temperature (°C)	Weibull $b \pm SE$	Weibull $n \pm SE$	R^2	MSE
10	35	0.02 ± 0.01	1.10 ± 0.11	0.960 - 0.982	0.00 - 0.04
	45	0.15 ± 0.04	0.86 ± 0.09		
	55	0.60 ± 0.06	0.55 ± 0.05		
20	45	0.09 ± 0.02	0.81 ± 0.07	0.920 - 0.972	0.01 - 0.10
	55	0.23 ± 0.08	0.80 ± 0.13		
	65	1.47 ± 0.18	0.31 ± 0.08		
30	45	0.01 ± 0.00	1.49 ± 0.25	0.801 - 0.916	0.04 - 0.13
	55	0.02 ± 0.03	1.48 ± 0.51		
	65	0.35 ± 0.10	0.86 ± 0.14		

*Strain NZRM 4447 (=ATCC 49025); b and n are Weibull scale and shape factors respectively; low mean square errors (MSE) and R^2 close to 1.00 are indication of good fit.

Table 2. First order kinetics parameters (D_T - and z_T -values) for *A. acidoterrestris* spores inactivation by 600 MPa HPP combined with mild heat in malt extract broth adjusted 10, 20 and 30°Brix.*

Soluble solids (°Brix)	HPP temperature (°C)	D_T -value \pm SE (min)	z_T -value \pm SE (°C)	R^2	MSE
10	35	38.08 \pm 1.24	20.82 \pm 2.17	0.829 - 0.980	0.00 - 0.10
	45	10.32 \pm 0.40			
	55	4.17 \pm 0.34			
20	45	21.63 \pm 0.98	20.07 \pm 1.01	0.508 - 0.948	0.02 - 0.53
	55	7.59 \pm 0.37			
	65	2.18 \pm 0.27			
30	45	32.26 \pm 2.07	21.43 \pm 2.52	0.703 - 0.909	0.03 - 0.17
	55	13.71 \pm 2.02			
	65	3.76 \pm 0.21			

*Strain NZRM 4447 (=ATCC 49025); low mean square error (MSE) and R^2 close to 1.00 are indication of good fit

Table 3. High pressure processing (HPP) at 600 MPa combined with 45°C: *A. acidoterrestris* spores resistance parameters in malt extract broth and the analog commercial juice/concentrate.*

Soluble solids (°Brix)	Media	First-order	Weibull	
		D_T (min) \pm SE	$b \pm$ SE	$n \pm$ SE
10	Malt extract broth	10.32 \pm 0.40	0.15 \pm 0.04	0.86 \pm 0.09
	Apple Juice	8.63 \pm 0.44	0.27 \pm 0.07	0.73 \pm 0.08
20	Malt extract broth	21.63 \pm 0.98	0.09 \pm 0.02	0.81 \pm 0.07
	Lime juice concentrate	19.88 \pm 1.15	0.10 \pm 0.05	0.81 \pm 0.14
30	Malt extract broth	32.26 \pm 2.07	0.01 \pm 0.00	1.49 \pm 0.25
	Blackcurrant juice concentrate	46.11 \pm 4.64	0.00 \pm 0.01	1.44 \pm 0.35

*Strain NZRM 4447 (=ATCC 49025)

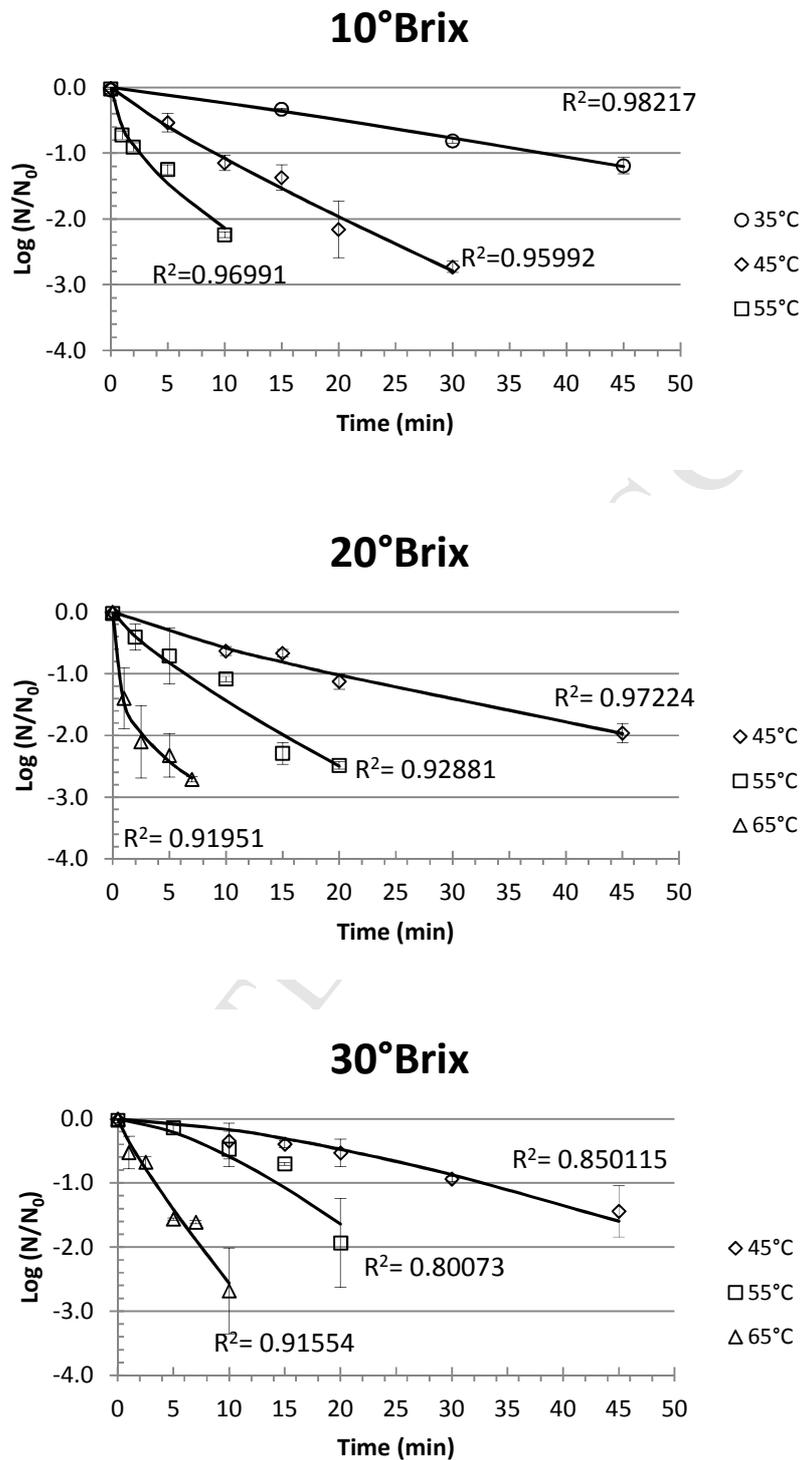


Figure 1. 600 MPa HPP combined with mild heat for the inactivation of *A. acidoterrestris* spores in malt extract broth adjusted 10, 20 and 30°Brix: effect of temperature and Weibull model fitting (values are log inactivation average \pm standard deviation).

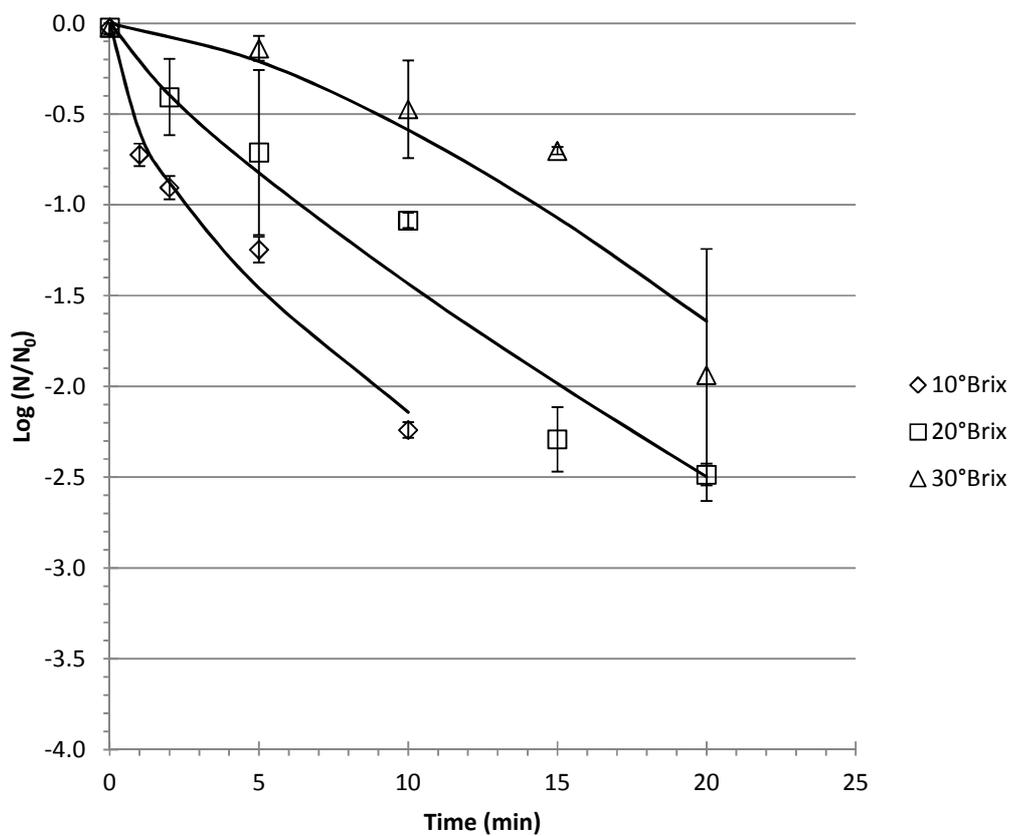


Figure 2. 600 MPa HPP combined with 55°C for the inactivation of *A. acidoterrestris* spores in malt extract broth adjusted 10, 20 and 30°Brix (values are average \pm standard deviation).

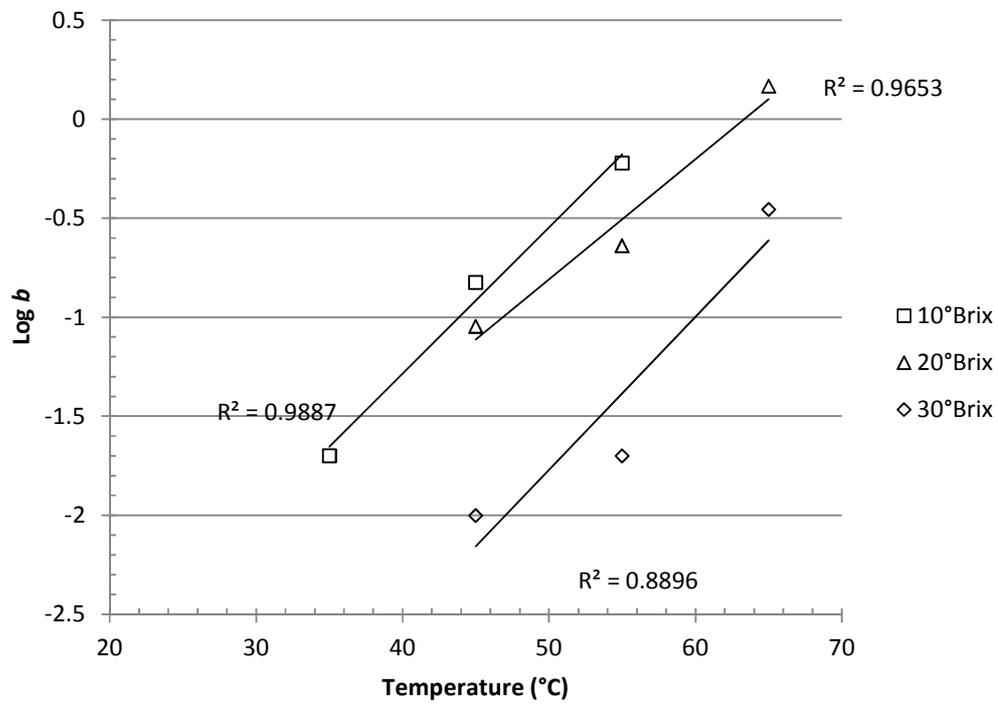


Figure 3. The effect of HPP temperature on the Weibull log *b* values for *A. acidoterrestris* spore inactivation at 600 MPa.

Highlights:

- HPP-thermal processing allows the use of lower pasteurization temperatures
- Higher soluble solids increased the resistance of *A. acidoterrestris* spores to HPP-thermal processes
- Weibull model described the nonlinear inactivation of *A. acidoterrestris* spores